

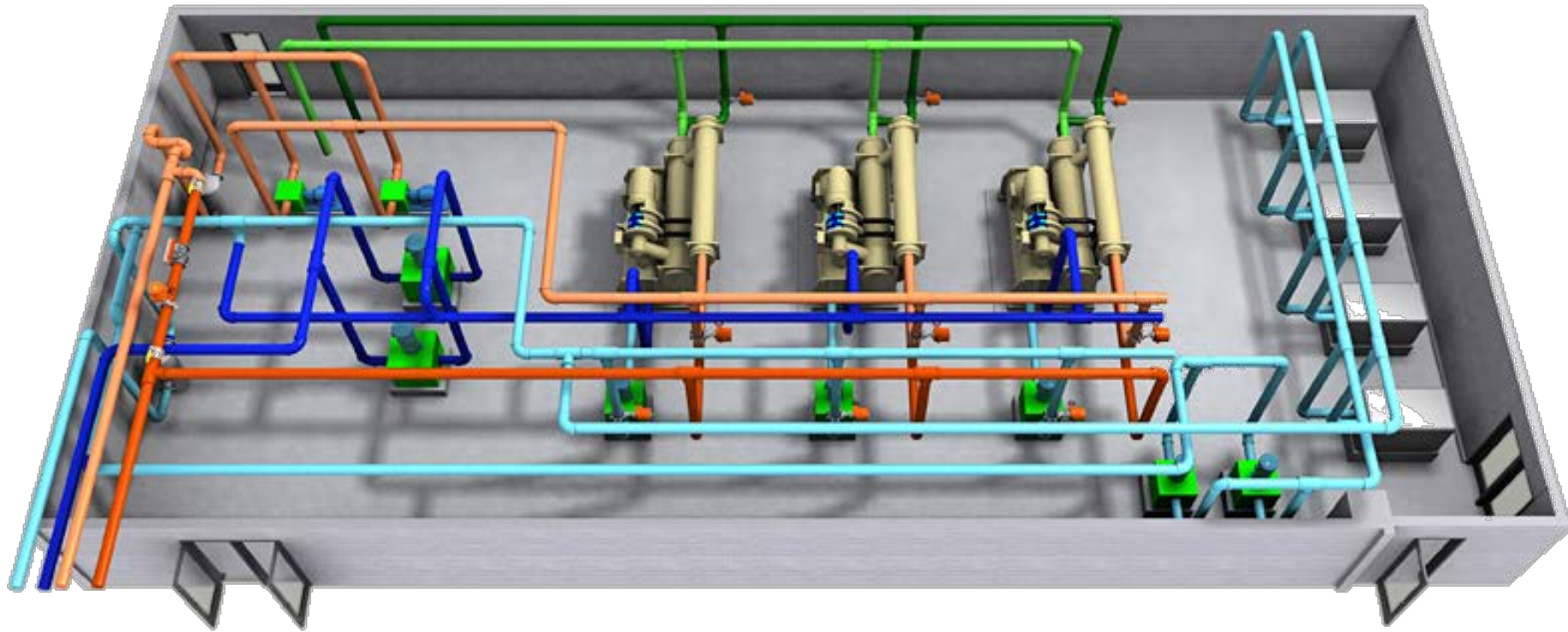


# High-performance Chilled-water Systems The Engineer's Role in Operation

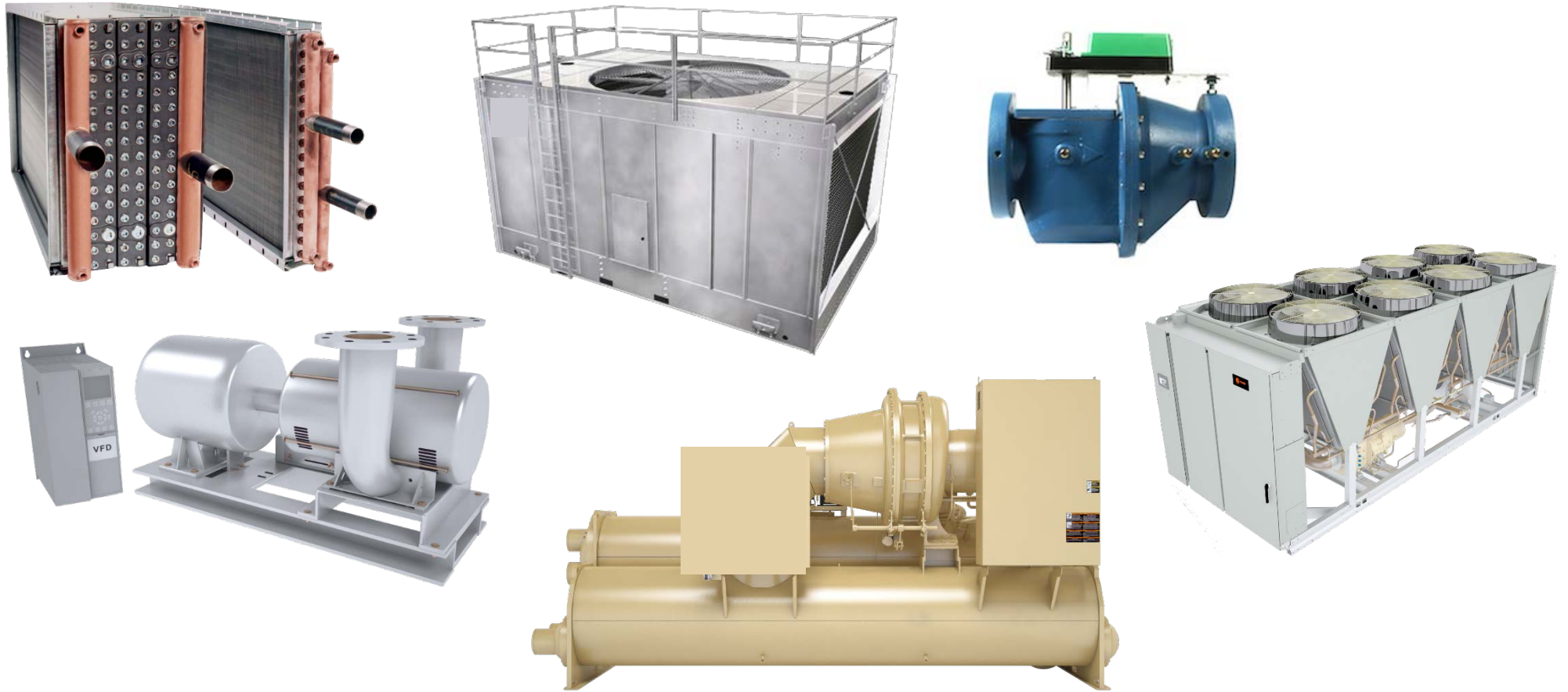
Susanna Hanson, CEM DGCP



# Chilled-water System



# Chilled-water System Components



# Connectivity





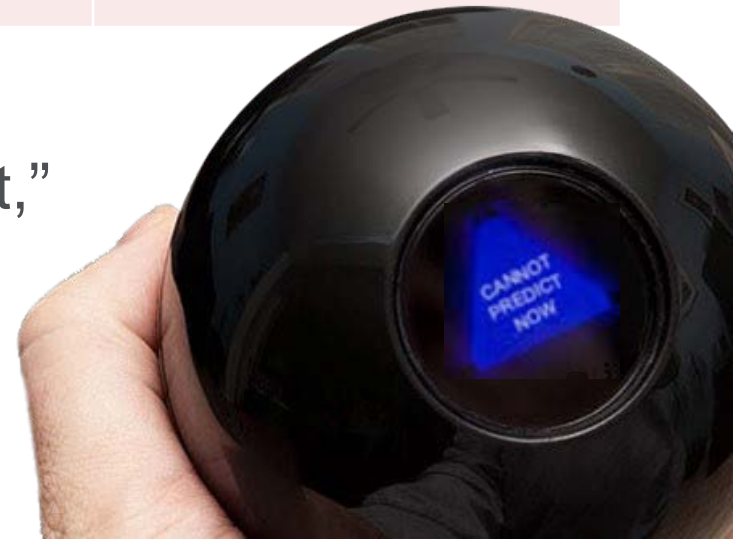
# Diagnostics



# Minimally-compliant Chiller Plant

Conventional assumption for code range		0.75-0.90 kW/ton (annual)
90.1-2010	Chillers + towers + CW pumps	.68-.88
90.1-2013	Chillers + towers + CW pumps	.66-.86

It's easy to model operation in what would have been deemed “excellent,” just by meeting code.



# Model $\neq$ Reality

- Assumption that flow perfectly varies with load
  - Coil performance assumptions
  - Hydronic dynamics ignored
  - Low delta T “syndrome”
  - Effect of valve instability on coil performance
  - If flow is unpredictable, so is pump energy
- Effects of above on equipment (pump and chiller) staging
  - Running more chillers (and pumps, and towers) than necessary
  - Chiller capacity assumed to follow load
    - Advanced models use a function of load and condensing pressure
    - None reduce chiller capacity based on low distribution delta T
- Simplified chilled water reset effects on chiller energy
  - No coil performance adjustments

**But Enough About Models**



# Effects of Responses to Discomfort

- Occupant
  - lower zone setpoint – increases GPM, may increase fan speed
  - supplement airflow – fans appear on or under desks
  - complain
- Operator
  - lower leaving air setpoint – decreases coil performance
  - pumps in manual, raise setpoint/speed – increases GPM, pressure
  - disable SA reset – lowers leaving air temp and increases reheat
  - reduce ventilation – lowers coil entering air temp, degrades coil perf
- All reduce system performance
  - Low delta T and poorer coil performance
  - Increase overcooling/reheat
  - “Out of flow-- out of chiller-- need another chiller...”
  - “Maybe I just need the system balancer back out here”
  - “We must need tertiary pumps”

# The Engineers' Dilemma

- Conservatism and unknowns
- Low pressure drop waterside
- Low pressure drop airside
- Fit in the box!
- Fit it in the budget!
- And we don't have money for reverse return piping
- Or pressure independent control valves
- Spend money for balancing valves and balancers!

# Step One: Pick the Right Heat Exchangers

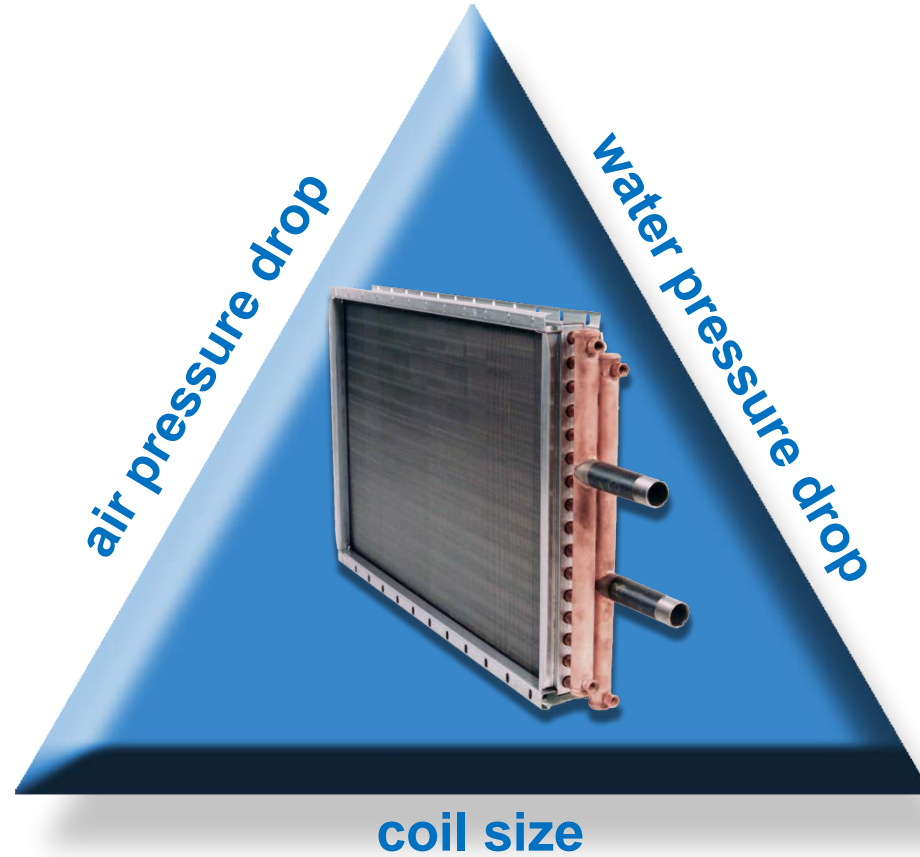
# Industry Recommendations

Source	Chilled Water $\Delta T$ (°F)	Condenser Water $\Delta T$ (°F)
ASHRAE 90.1-2016 requirement	$\geq 15$	NA
ASHRAE GreenGuide	12 - 20	12 - 18
Kelly and Chan	18	14
Taylor	$> 12$	15

# Chilled Water Optimizations – ASHRAE 90.1

- Coil selection for 15°F DT or higher (57°F min return)
- and-
- Chilled water reset based on critical valve position
- or-
- Pump pressure reset based on critical valve position

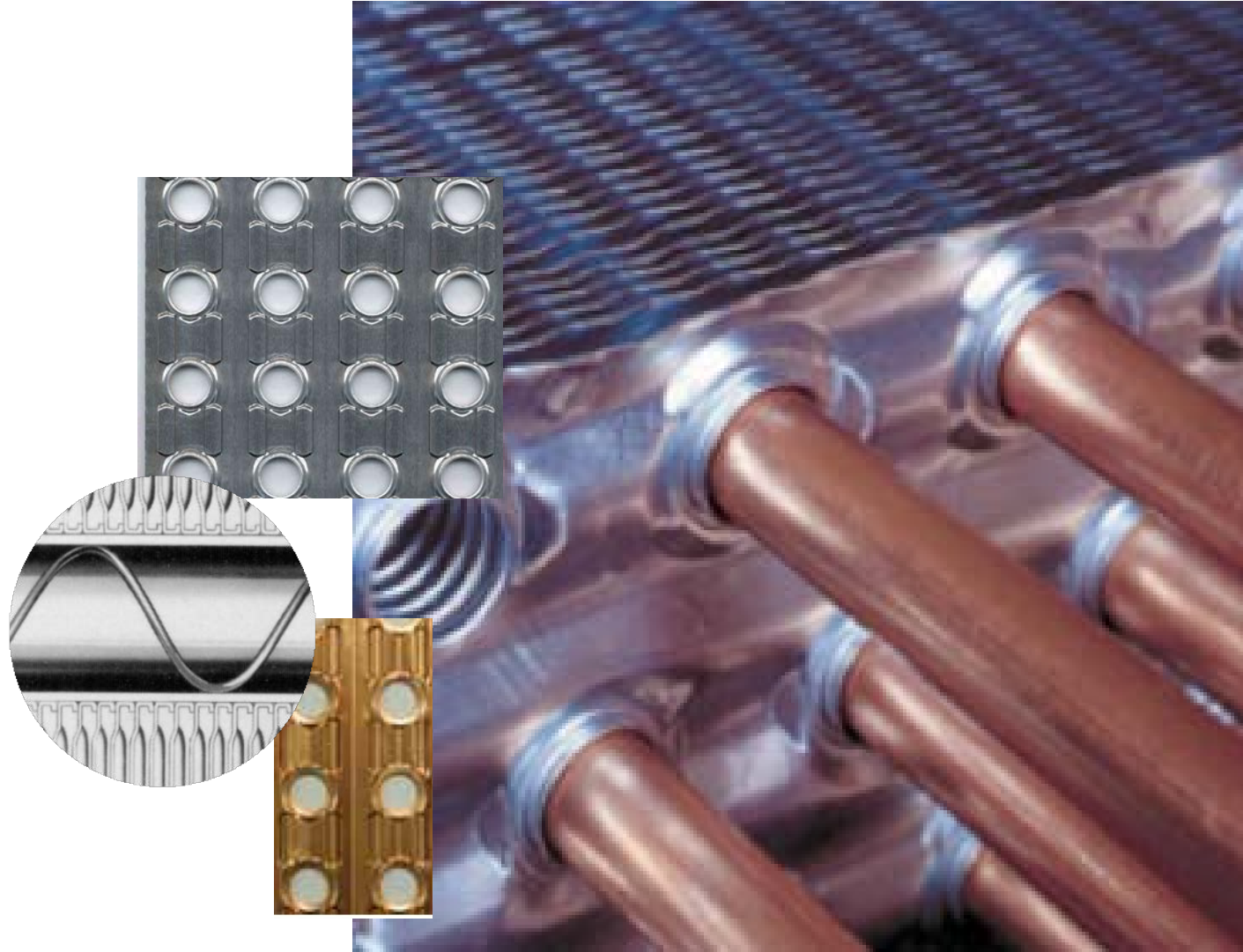
# Coil Selection: APD versus WPD versus Size





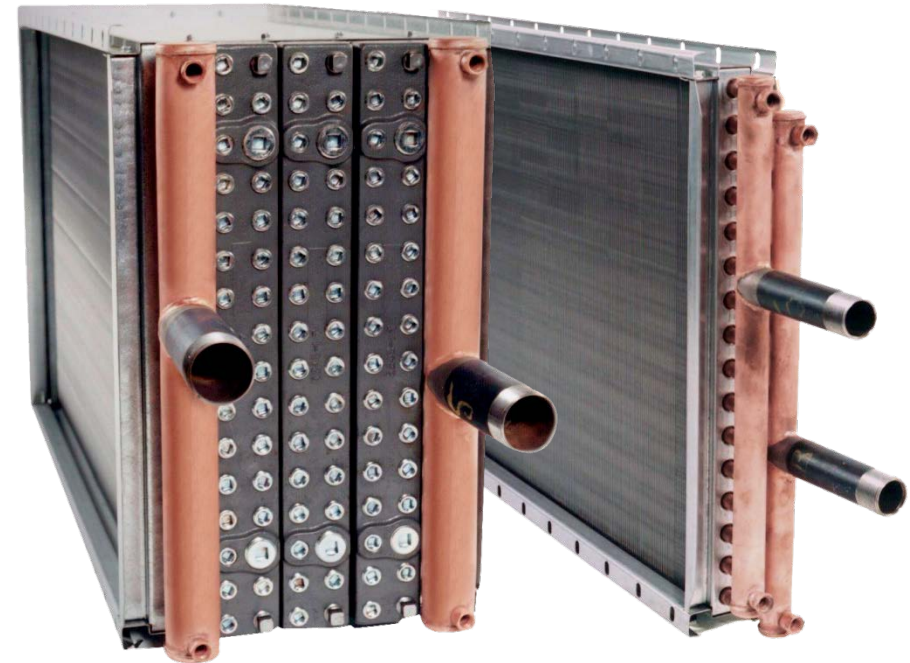
# Configuration Options

- Coil face area
- Number of rows of tubes
- Tube diameter
- Number of fins
- Fin surface design
- Coil circuiting
- Turbulators



# Construction Options

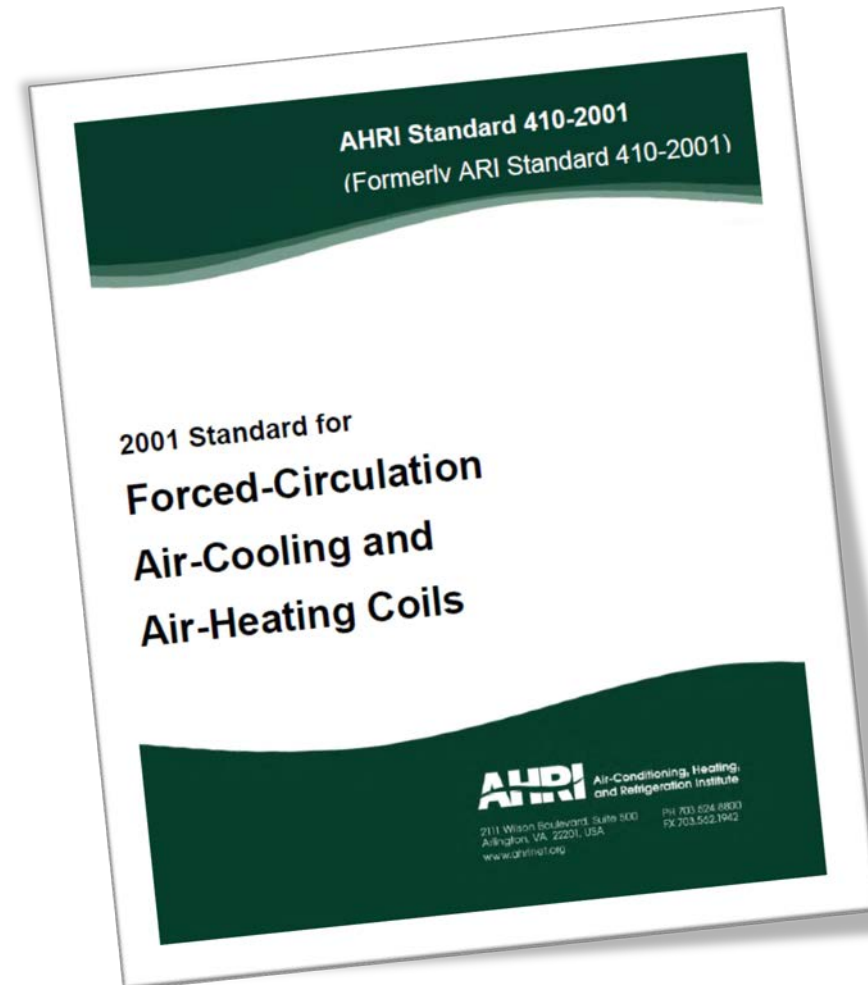
- Tube material
- Tube wall thickness
- Fin material
- Fin thickness
- Casing material
- Header type and material
- Coil coatings



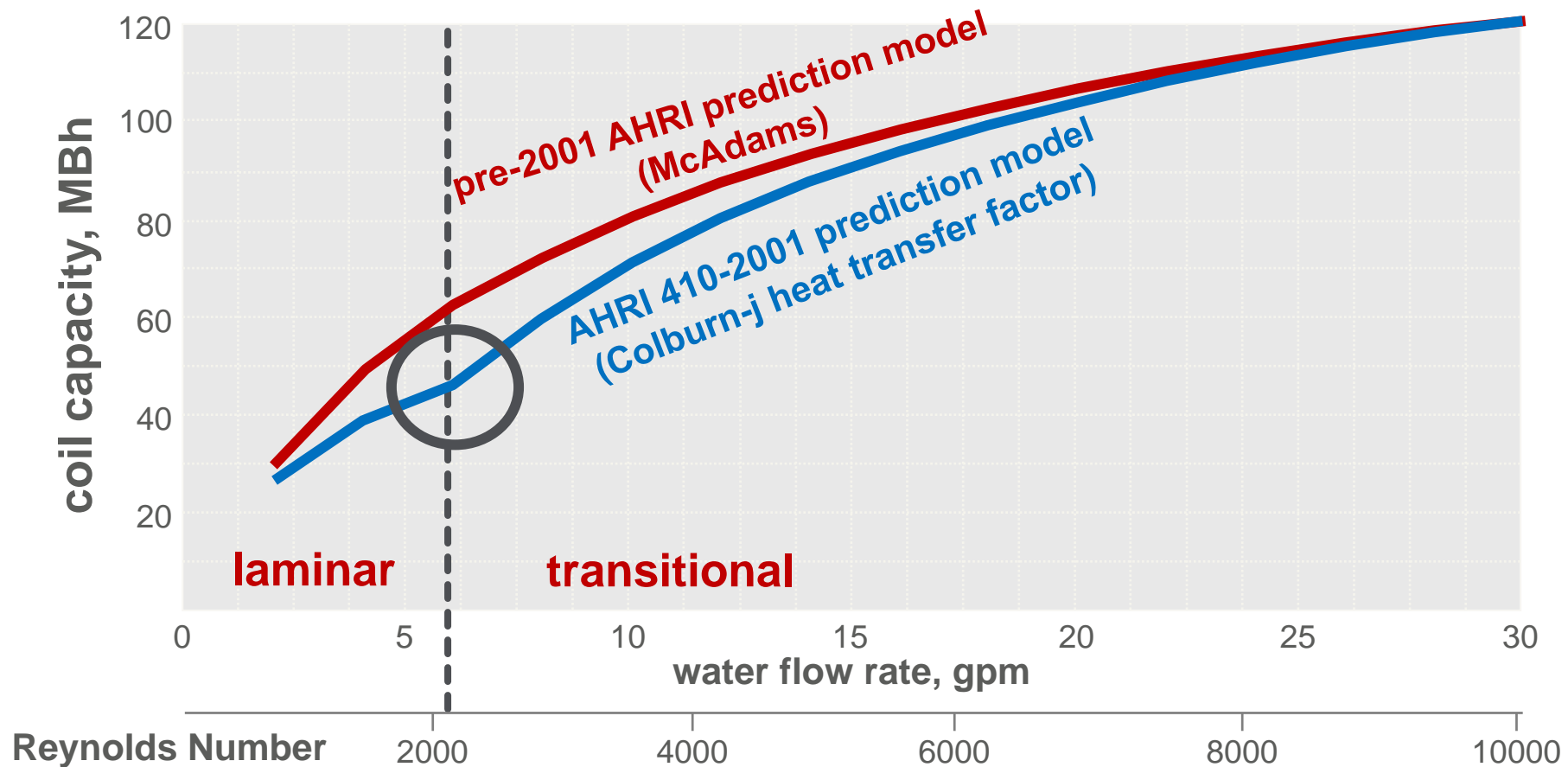
# Coil Certification Program

## AHRI Standard 410

*Forced-Circulation Air-Cooling  
and Air-Heating Coils*



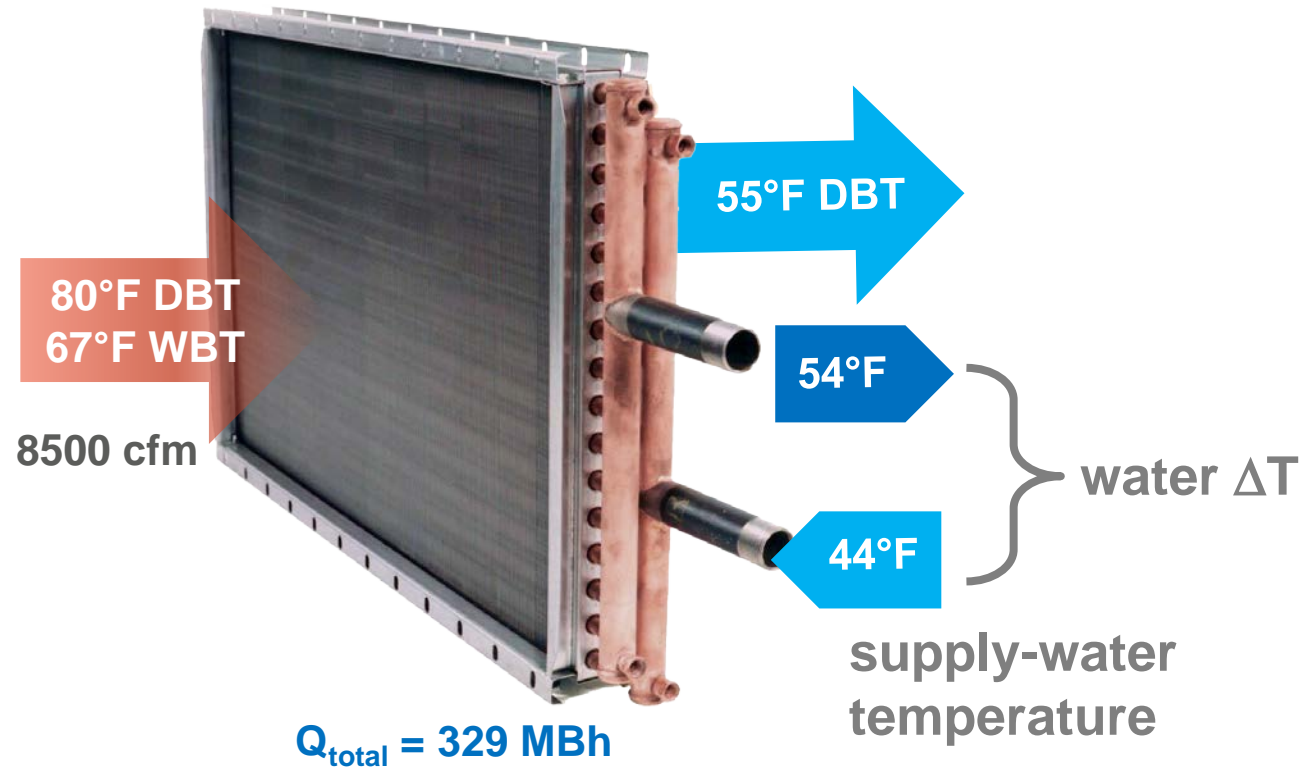
# Laminar Flow $\neq$ Severe Capacity Drop-off



# Conserve Energy Transporting Tons

- $Tons = \frac{(\Delta T \times GPM)}{24}$
- Solving for gpm...
- $GPM = \frac{(Tons \times 24)}{\Delta T}$
- Pumping power...
- Frictional Head ; Flow 2
- $Water\ HP\ (bhp) = \frac{(GPM \times head\ (ft))}{3960}$
- Water HP ; Flow <sup>3</sup>; Delta T <sup>3</sup>

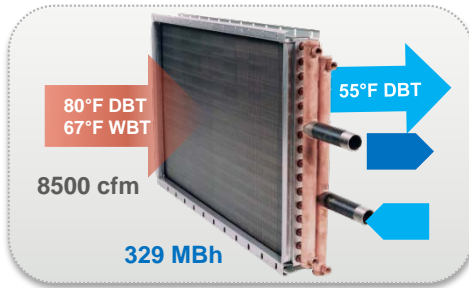
# Supply-Water Temp and $\Delta T$



Lowest Cost?  
Lowest Energy?  
Neither

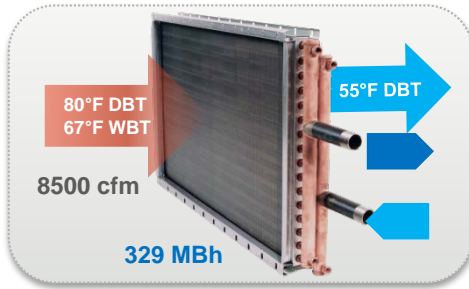


# Supply-Water Temp and $\Delta T$



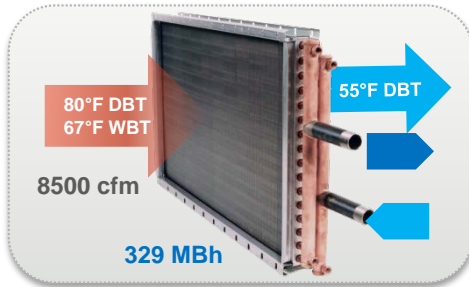
coil face area, ft <sup>2</sup>	17	17
coil rows	6	6
coil fins, fins/ft	95	127
supply water temperature, °F	44	44
return water temperature, °F	54	57
water $\Delta T$ , °F	10	13
water flow rate, gpm	65.6	50.4
water velocity, ft/sec	3.6	2.8
water pressure drop, ft H <sub>2</sub> O	8.2	5.1
air pressure drop, in H <sub>2</sub> O	0.68	0.77
cost of the coil	base	base + 7%

# Supply-Water Temp and $\Delta T$



coil face area, ft <sup>2</sup>	17	17	17
coil rows	6	6	6
coil fins, fins/ft	95	127	99
supply water temperature, °F	44	44	42
return water temperature, °F	54	57	55
water $\Delta T$ , °F	10	13	13
water flow rate, gpm	65.6	50.4	50.4
water velocity, ft/sec	3.6	2.8	2.8
water pressure drop, ft H <sub>2</sub> O	8.2	5.1	5.1
air pressure drop, in H <sub>2</sub> O	0.68	0.77	0.68
cost of the coil	base	base + 7%	base + 1%

# Supply-Water Temp and $\Delta T$



coil face area, ft <sup>2</sup>	17	17	17	17
coil rows	6	6	6	4
coil fins, fins/ft	95	127	99	141
supply water temperature, °F	44	44	42	40
return water temperature, °F	54	57	55	56
water $\Delta T$ , °F	10	13	13	16
water flow rate, gpm	65.6	50.4	50.4	41.0
water velocity, ft/sec	3.6	2.8	2.8	2.3
water pressure drop, ft H <sub>2</sub> O	8.2	5.1	5.1	5.8
air pressure drop, in H <sub>2</sub> O	0.68	0.77	0.68	0.56
cost of the coil	base	base + 7%	base + 1%	base – 16%

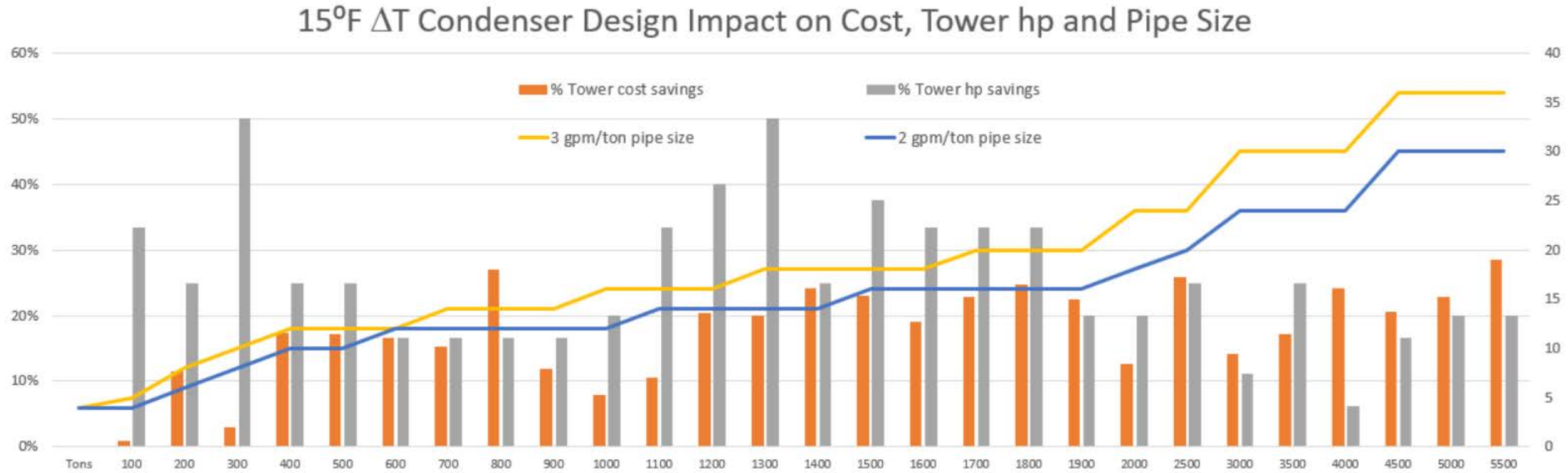
# Going for Best Energy Efficiency?

entering water temp, °F	42	42	40
leaving water temp, °F	57	62	65
water $\Delta T$ , °F	15	20	25
tube diameter, in.	1/2	1/2	1/2
rows	6	8	8
fin density, fins/ft	124	114	135
fin design	high eff	high eff	high eff
turbulators	yes	yes	yes
water flow rate, gpm	40	30	24
water velocity, ft/sec	2.8	2.1	1.6
water pressure drop, ft. H <sub>2</sub> O	11.1	8.4	5.8
air pressure drop, in. H <sub>2</sub> O	0.71	0.88	0.92
cost of coil	base	base + 29%	base + 34%

# What Does High Delta T “Unlock”

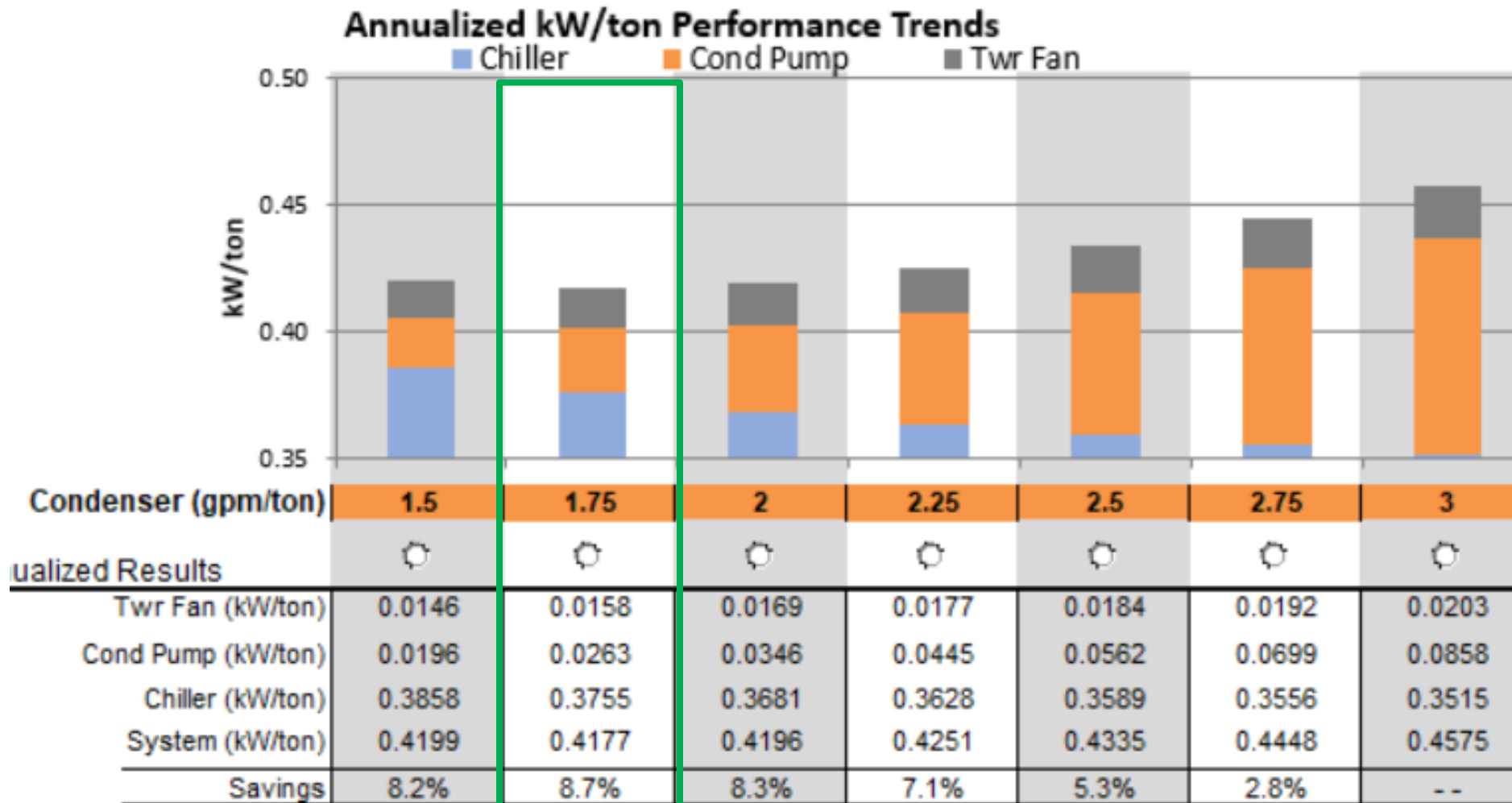
- Heat recovery
  - Warmer return water lets us fully load the chillers = more free heat
- Series chillers
  - If we can't get the DT we can't load the chillers
- Longer economizer
  - Warmer return water temperature can be cooled by towers alone
- Chilled water storage
  - DT is the most critical factor in economics and operational success of chilled water storage
- Retrofits (pipes too small, expansion without more electrical, physical size)

# 15°F $\Delta T$ Works On Condenser Side Too – Cost





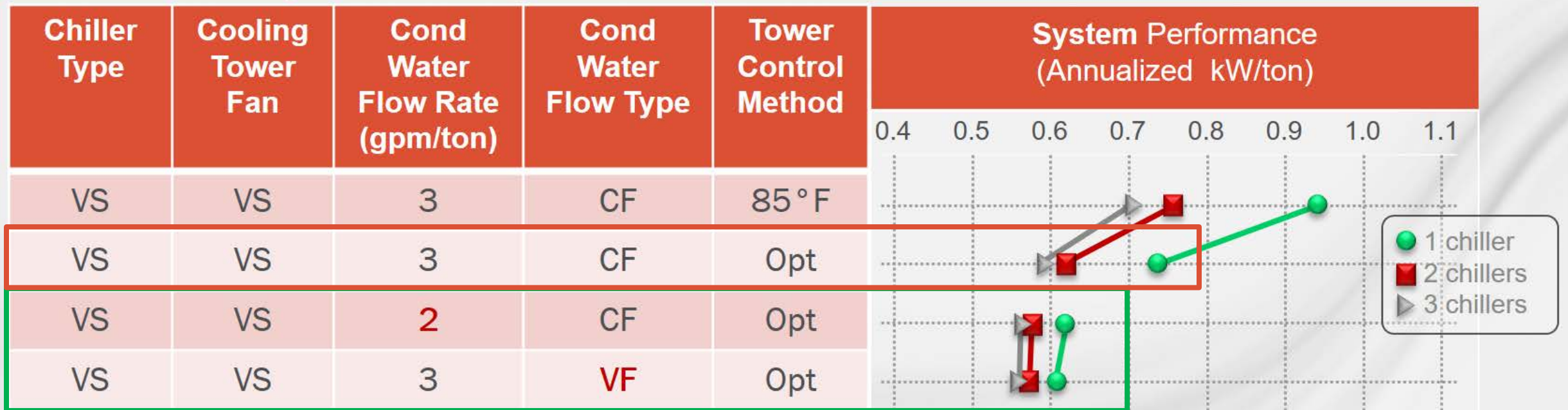
# 15°F ΔT For Tower and Chiller HX Too – Energy



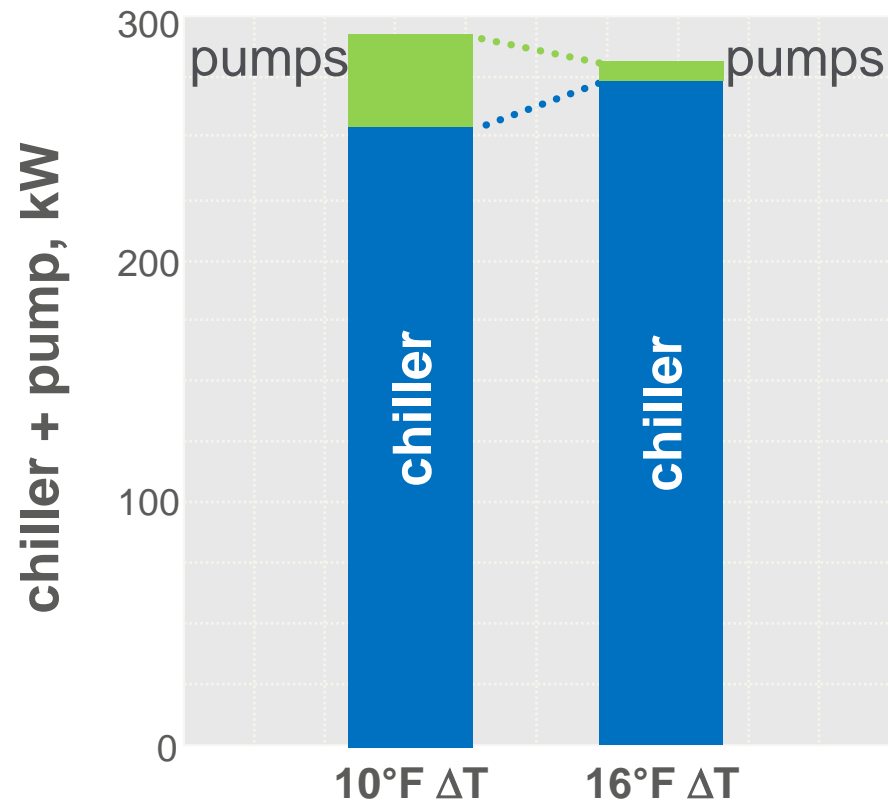
# 15°F ΔT For Tower and Chiller HX Too – Energy

Controls are more persistent with low flow all the time

## Annualized System Performance



# Higher $\Delta T$ Chilled Water Systems



# Operation

# Low Delta-T (High Flow) Syndrome

- Symptom of poor design and operation
- Excessive energy
  - Excessive pump energy
  - Excessive fan energy
  - Excessive chiller energy
- Decreased comfort
  - Degrades dehumidification and temperature control
- Decreased Capacity
  - Running out of chilled water capacity
  - “My Pipes Is Out of Tons”

## Why is Low Delta T Bad?

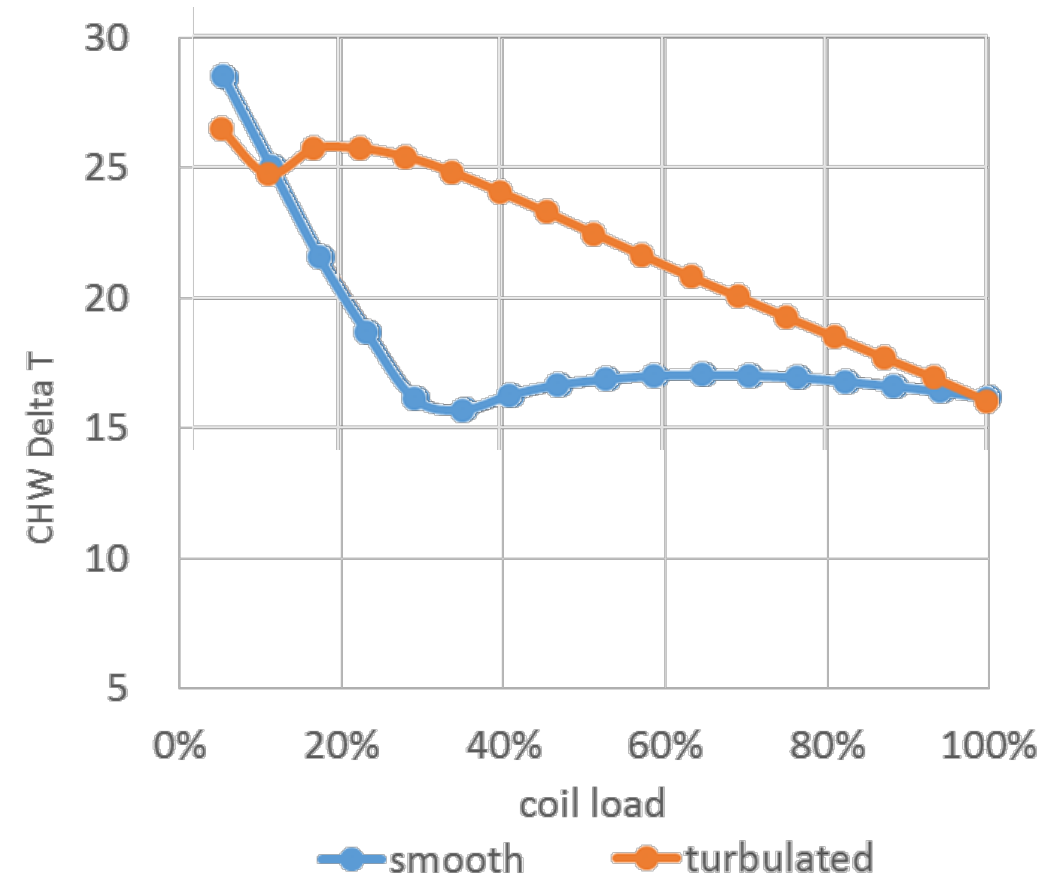
- Tough to model = tough business case
- Chillers get blamed
- Fouling gets blamed
- Filters get blamed
- System balancer gets blamed
- Engineer gets blamed
- Customers and occupants unhappy



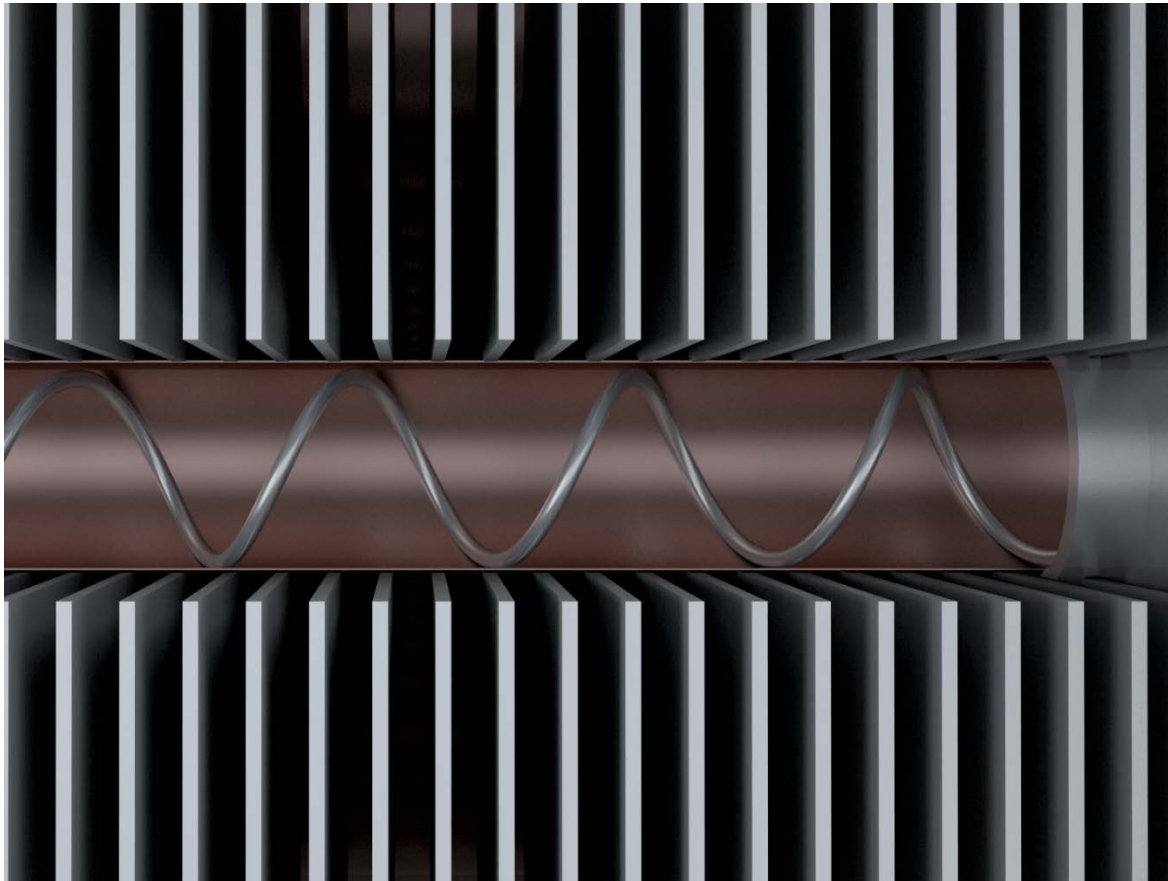
# Yes BUT, Coil Delta T is lower at Part Load

Is it physics or is it something else?

- AHRI Certified Coil
- Air Flow (VAV) unloading



## Turbulators Help Maintain $\Delta T$ at Reduced Flows

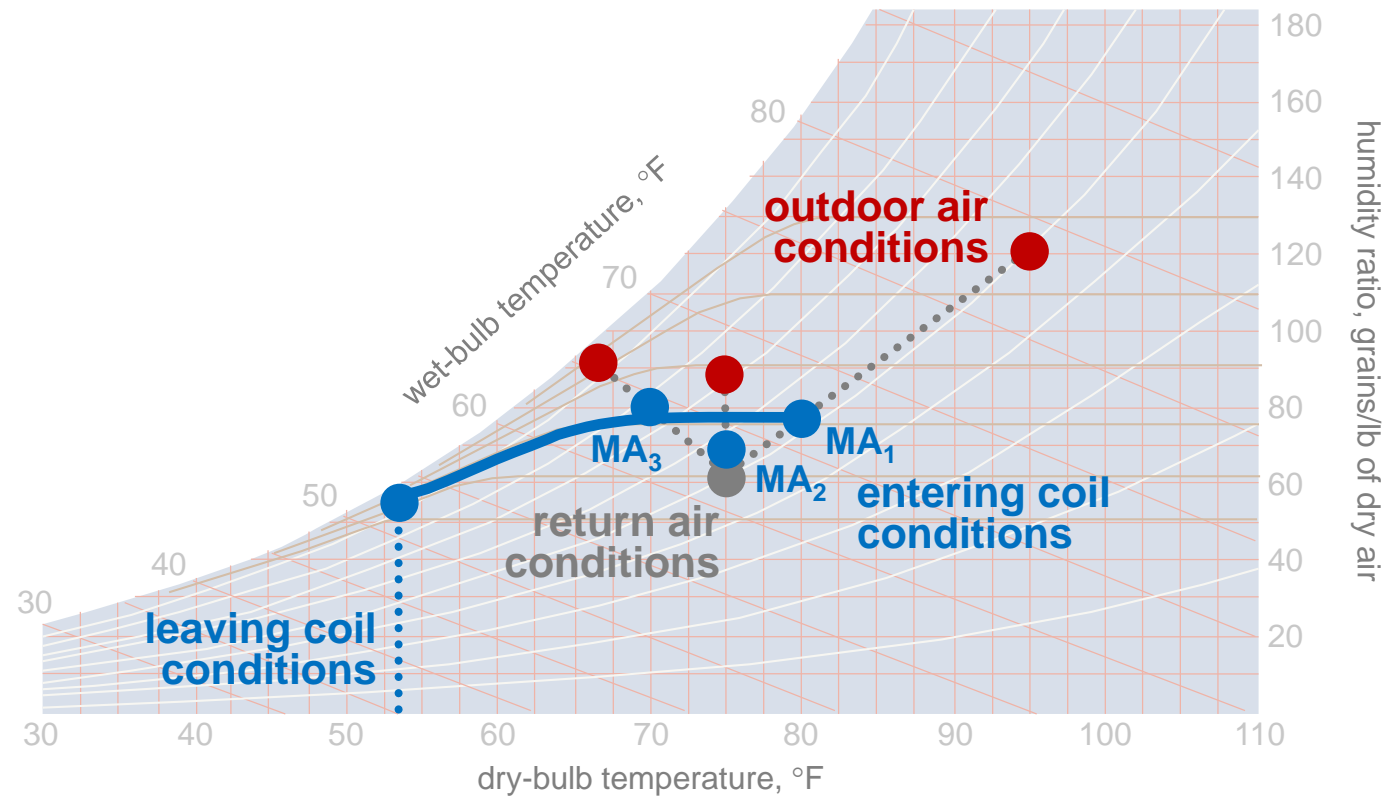


Turbulators...

- Increase fluid turbulence, which improves heat transfer
- Allows coil to provide required capacity with a lower GPM

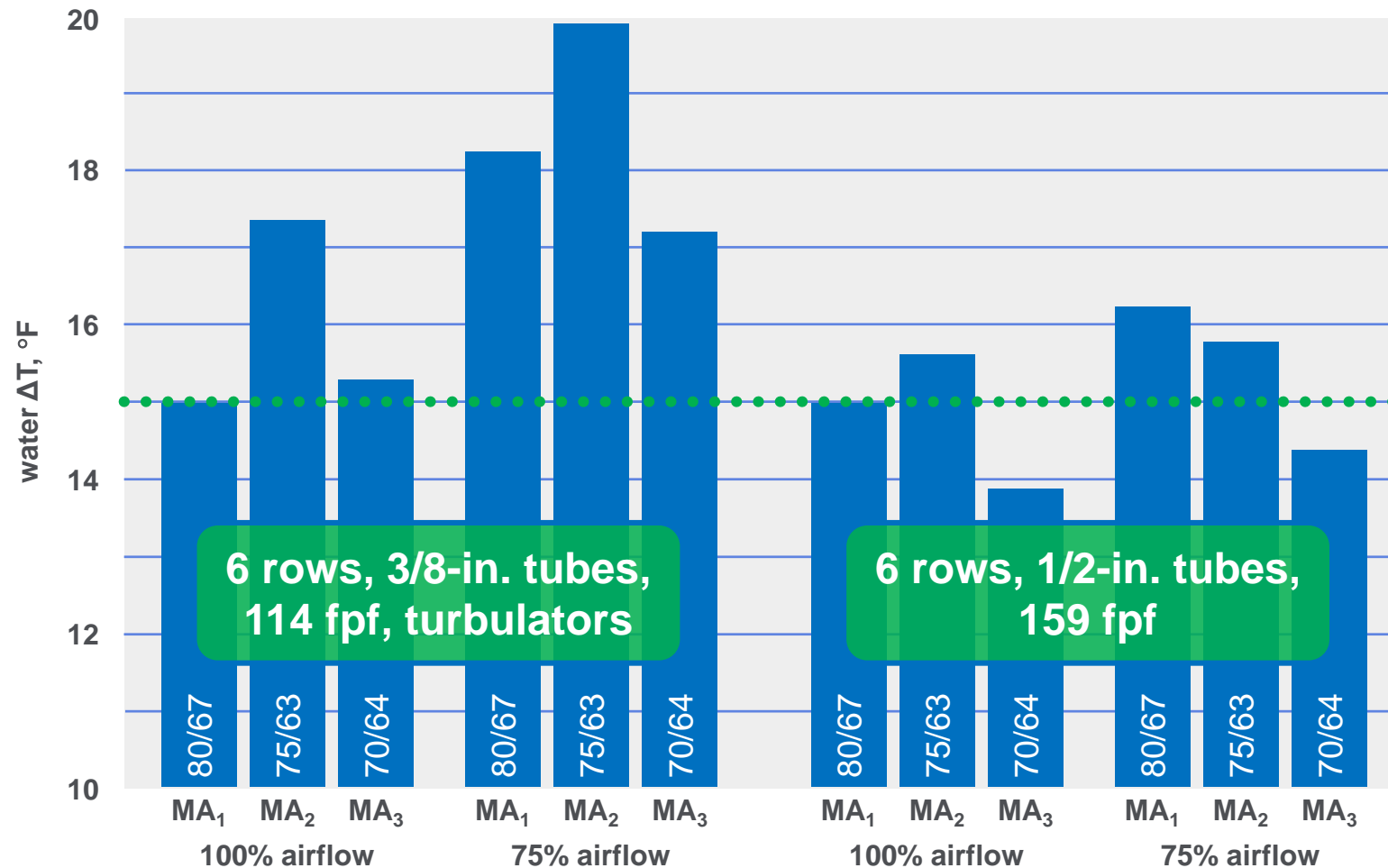
# Coil Conditions Change @ Part Load

## Impact of Entering Air Temps, Lower Airflow on $\Delta T$



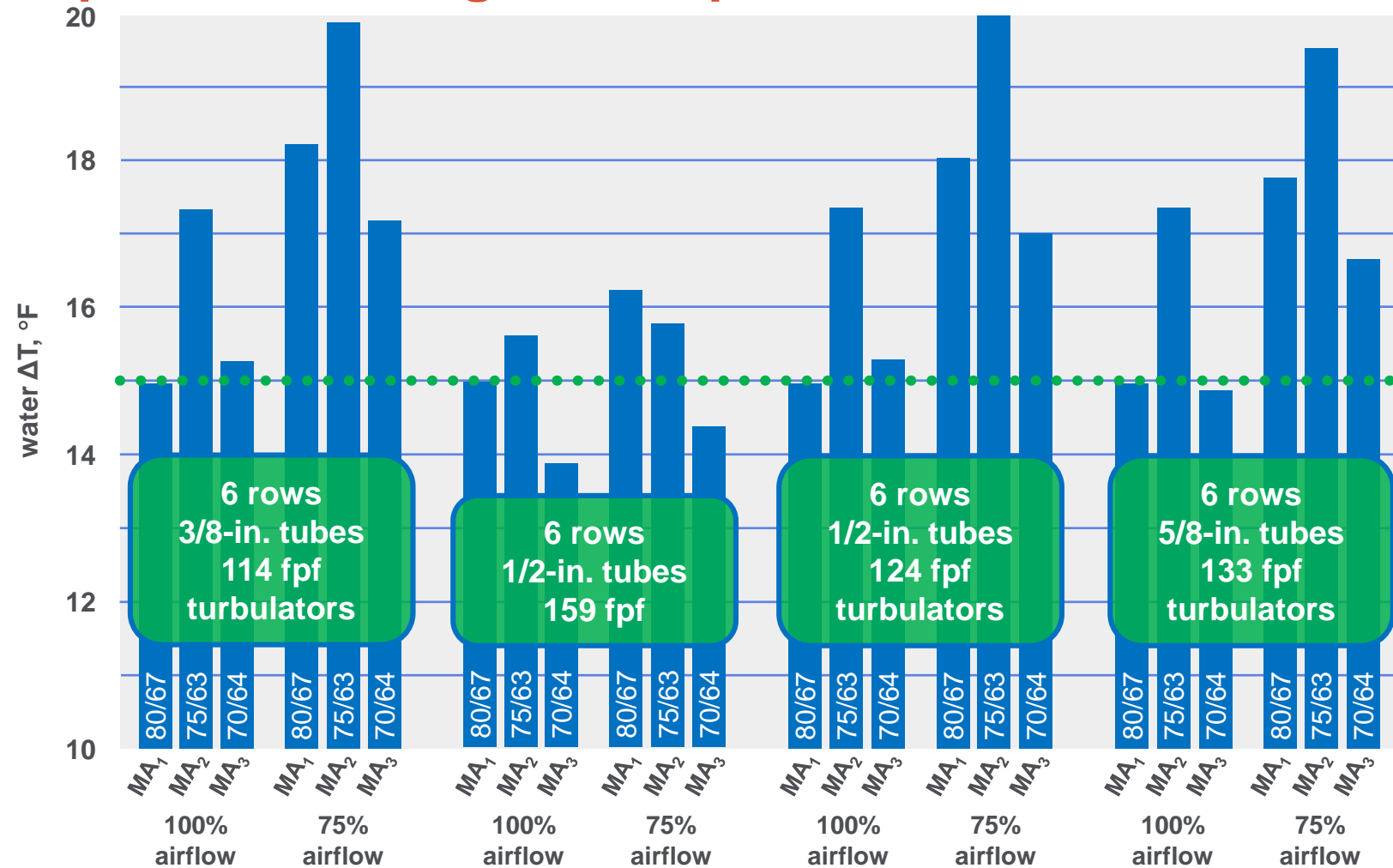
# Coil Conditions Change @ Part Load

## Impact of Entering Air Temps, Lower Airflow on $\Delta T$



# Coil Conditions Change @ Part Load

## Impact of Entering Air Temps, Lower Airflow on $\Delta T$



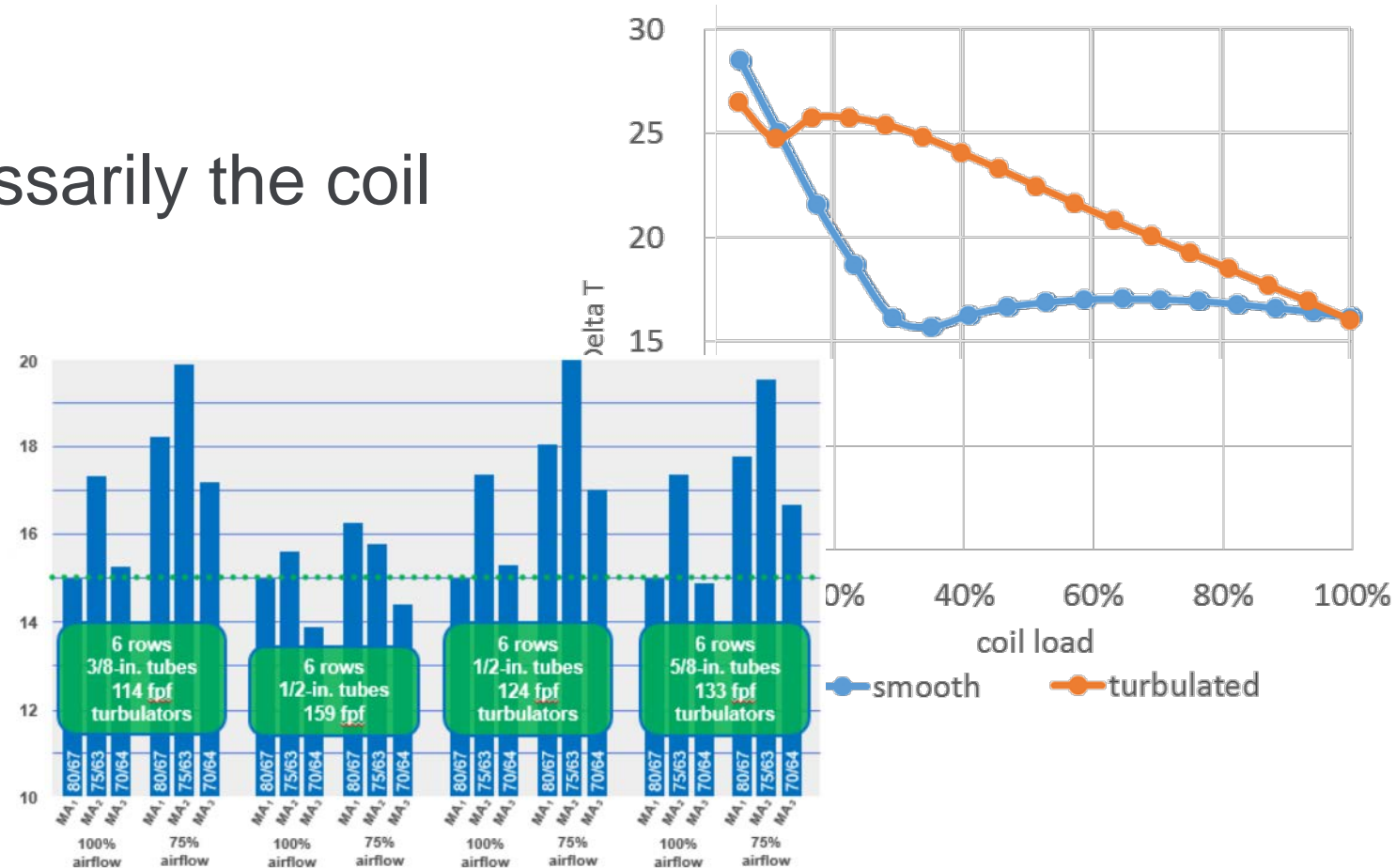
## Coil Selection Cost, Fan and Pump Energy

entering water temp, °F	42	42	42	42
leaving water temp, °F	57	57	57	57
water $\Delta T$ , °F	15	15	15	15
tube diameter, in.	3/8	1/2	1/2	5/8
rows	6	6	6	6
fin density, fins/ft	114	159	124	133
fin design	high cap	high cap	high eff	high eff
turbulators	yes	no	yes	yes
water flow rate, gpm	40	40	40	40
water velocity, ft/sec	2.7	2.8	2.8	2.1
water pressure drop, ft. H <sub>2</sub> O	11.2	4.7	11.1	5.2
air pressure drop, in. H <sub>2</sub> O	0.81	0.95	0.71	0.71
cost of coil	base - 30%	base	base + 8%	base + 15%

# So WHY, is System Delta T Low?

Is it physics or is it something else?

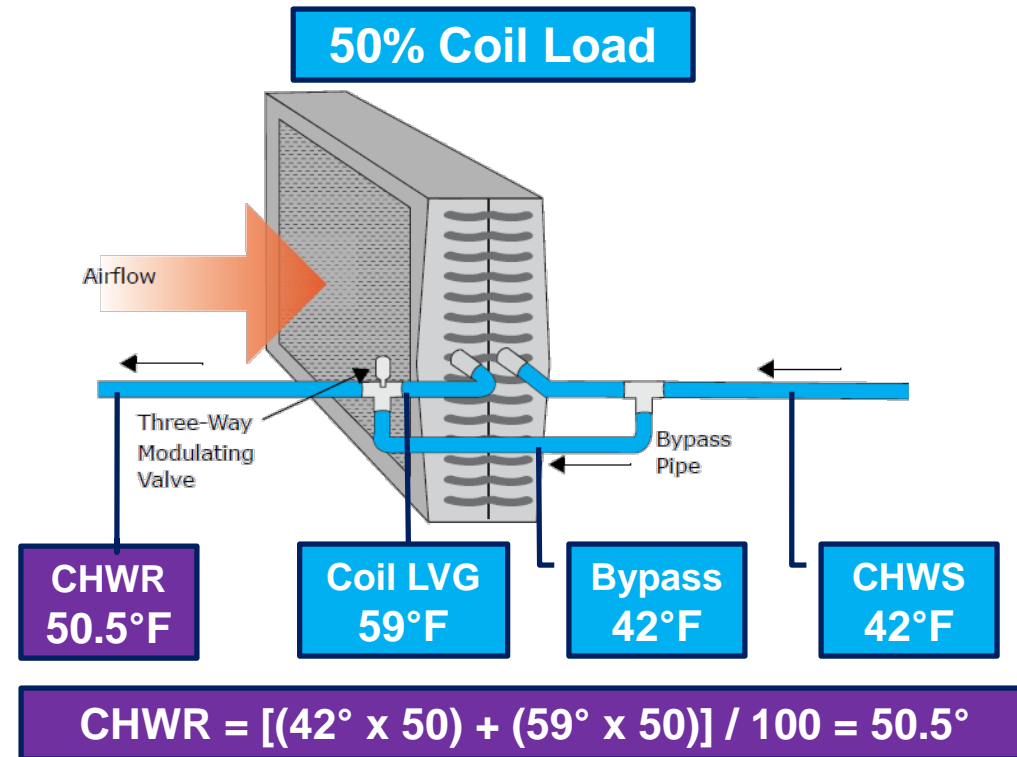
It's not necessarily the coil



## Reason 1: 3-Way control valves undesirable mixing in variable flow systems

- *Eliminate them!*

Coil Delta T = 17°F  
System Delta T = 8.5°F





## Reason 2: Supply air setpoint depression overdriving coil capacity

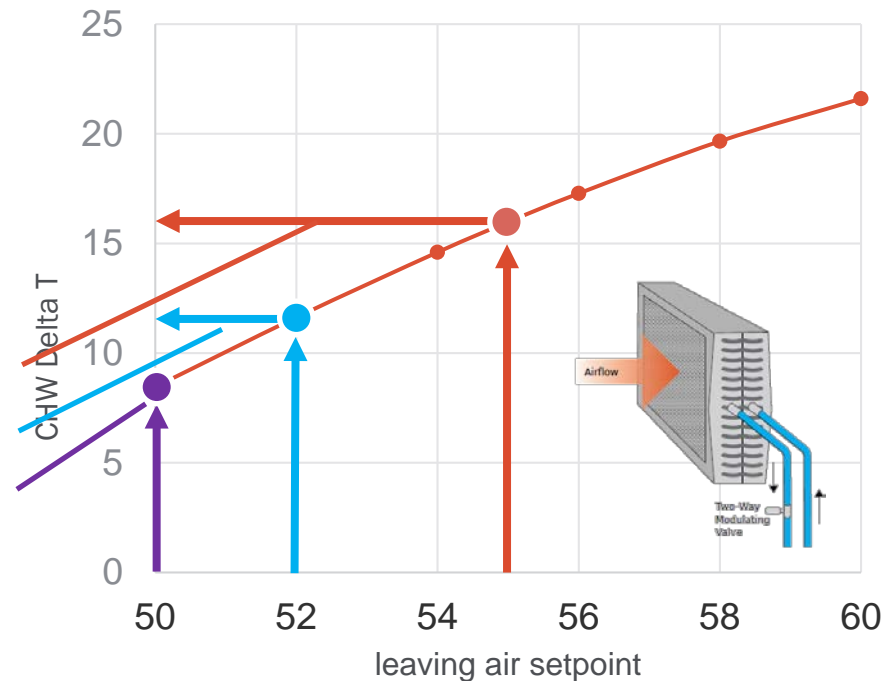
1. 3-way control valves
2. Control setpoint depression

- *Avoid, limit and restore*

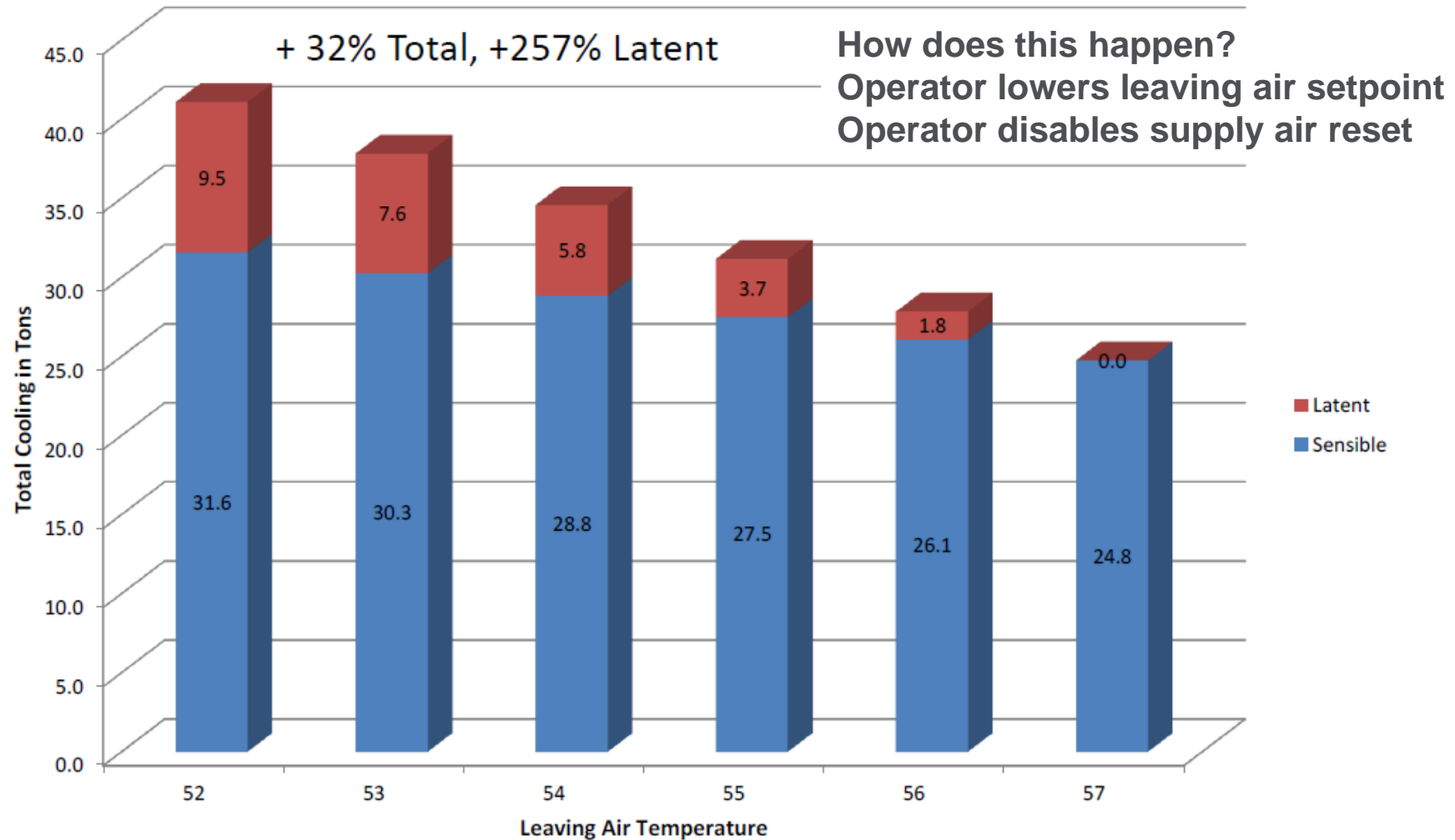
55° LAT = 16° DT = 1.5 gpm/ton 🙄

52° LAT = 11° DT = 2.2 gpm/ton 🙄

50° LAT = 8.5° DT = 2.8 gpm/ton 🙄



# Overdriving Coil Capacity



## Reason 3: Warmer chilled water supply

reduced heat transfer driving force “LMTD”

1. 3-way control valves
2. LAT setpoint depression

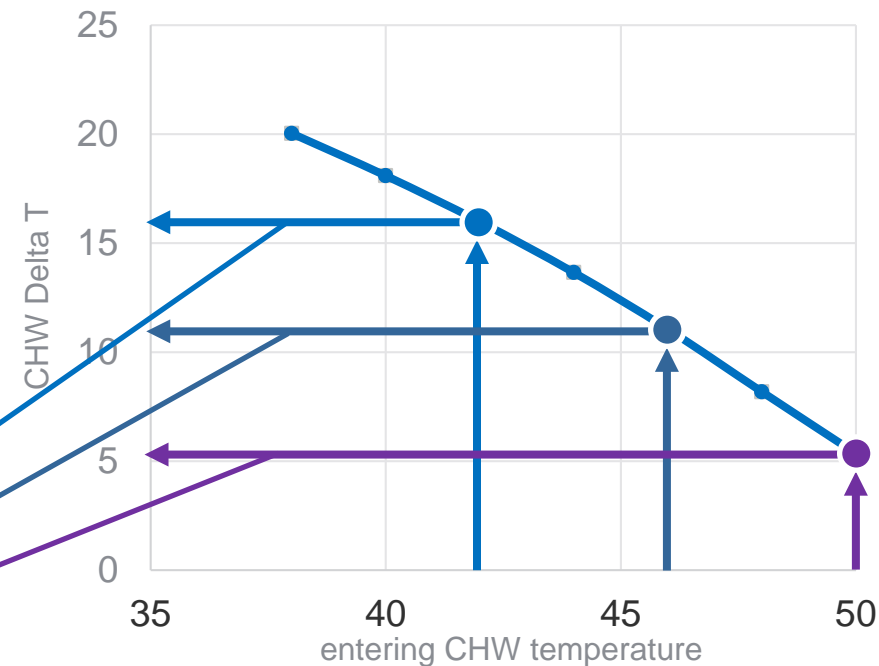
### 3. Warmer chilled water

- *Chilled water reset only at part load*

42° CHWS = 16° DT = 1.5 gpm/ton 🤔

47° CHWS = 7.5° DT = 3.2 gpm/ton 🤔

50° CHWS = 5° DT = 4.8 gpm/ton 🤔



**CHW reset OK in high DT designs  
and at chiller min flow in VPF system**

# Reason 4: Deficient control valves

poor flow control at full and part loads

1. 3-way control valves
2. LAT setpoint depression
3. Warmer chilled water
4. Deficient control valves

## Control Valve Issues

1. Improperly Selected / Oversized
2. Worn-out
3. Unstable control
4. \$29.95 (cheap)
5. 3-way valves

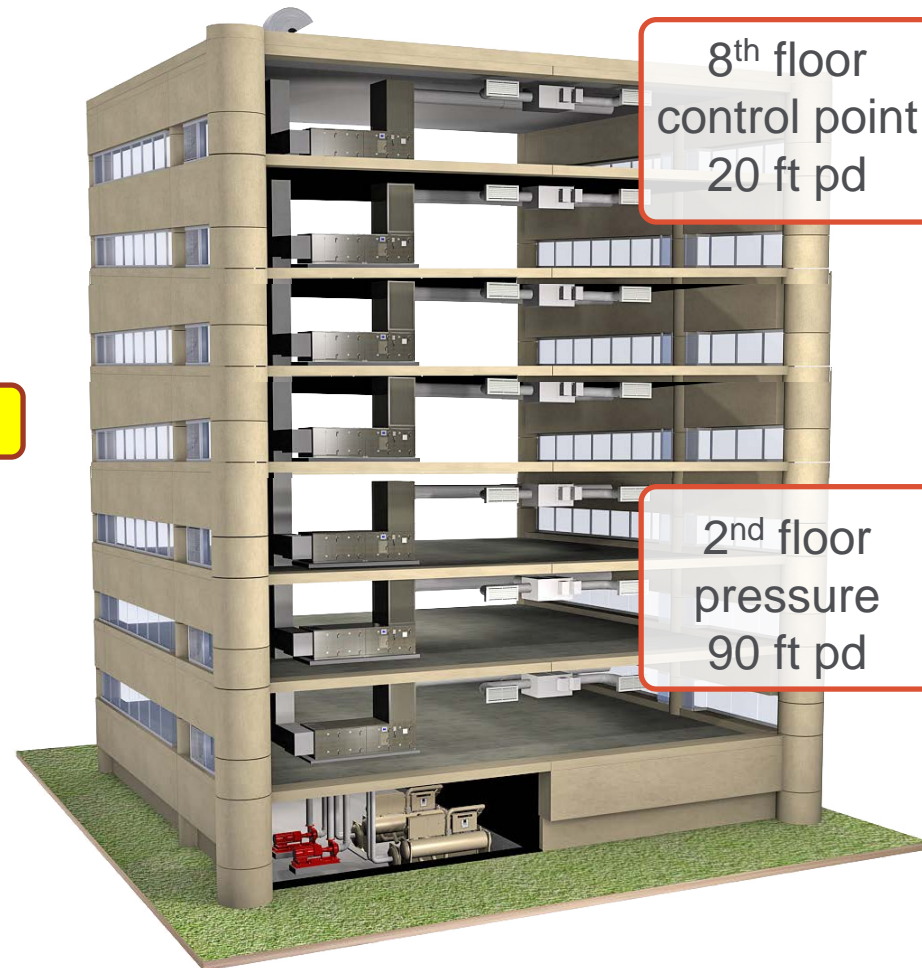


# Reason 4: Deficient control valves

poor flow control

1. 3-way control valves
2. LAT setpoint depression
3. Warmer chilled water
4. Deficient control valves

- *Specify quality valves specific to use*



# Reason 4: Deficient control valves

poor flow control

1. 3-way control valves
2. LAT setpoint depression
3. Warmer chilled water
4. Deficient control valves

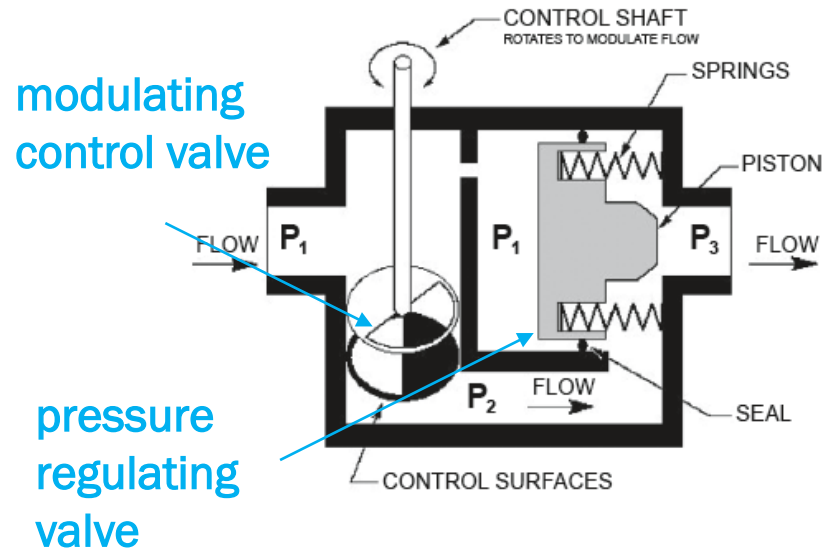
Pressure independent valves? (PICV)

- Not always required
  - Reverse return piping can help
  - Cures many problems
1. Mechanical
  2. Electronic

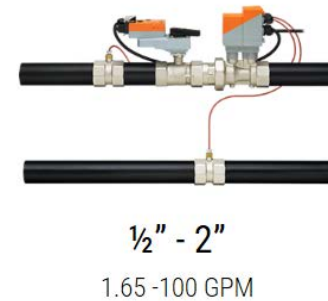


# Pressure Independent Control Valves

mechanical PI valve



electronic PI valve

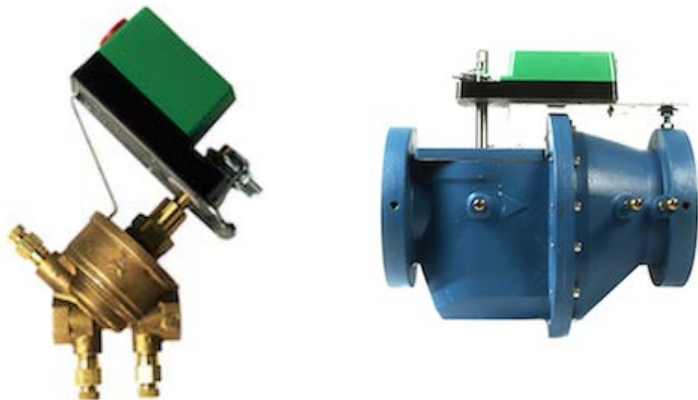


- More stable and accurate
  - Increased delta T
- Easier to select
- Easier to install
- May be cost neutral

# PIC Valves

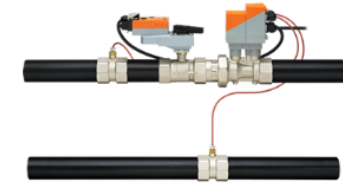
## Mechanical

- More compact
- Will accept any rotary actuator
- Easier to select
- No additional power, programming, or sensor installation
- Now available with data sharing



## Electronic

- Potential for lower hardware costs
- Provides load measurement
- Programmable for various operation methods:
  - Flow limiting
  - $\Delta T$  limiting
  - Energy limiting
- BACnet™ Communication to BAS system for data sharing.  
(requires licensing and commissioning another BACnet device)



½" - 2"

1.65 -100 GPM



2½" - 6"

80-713 GPM

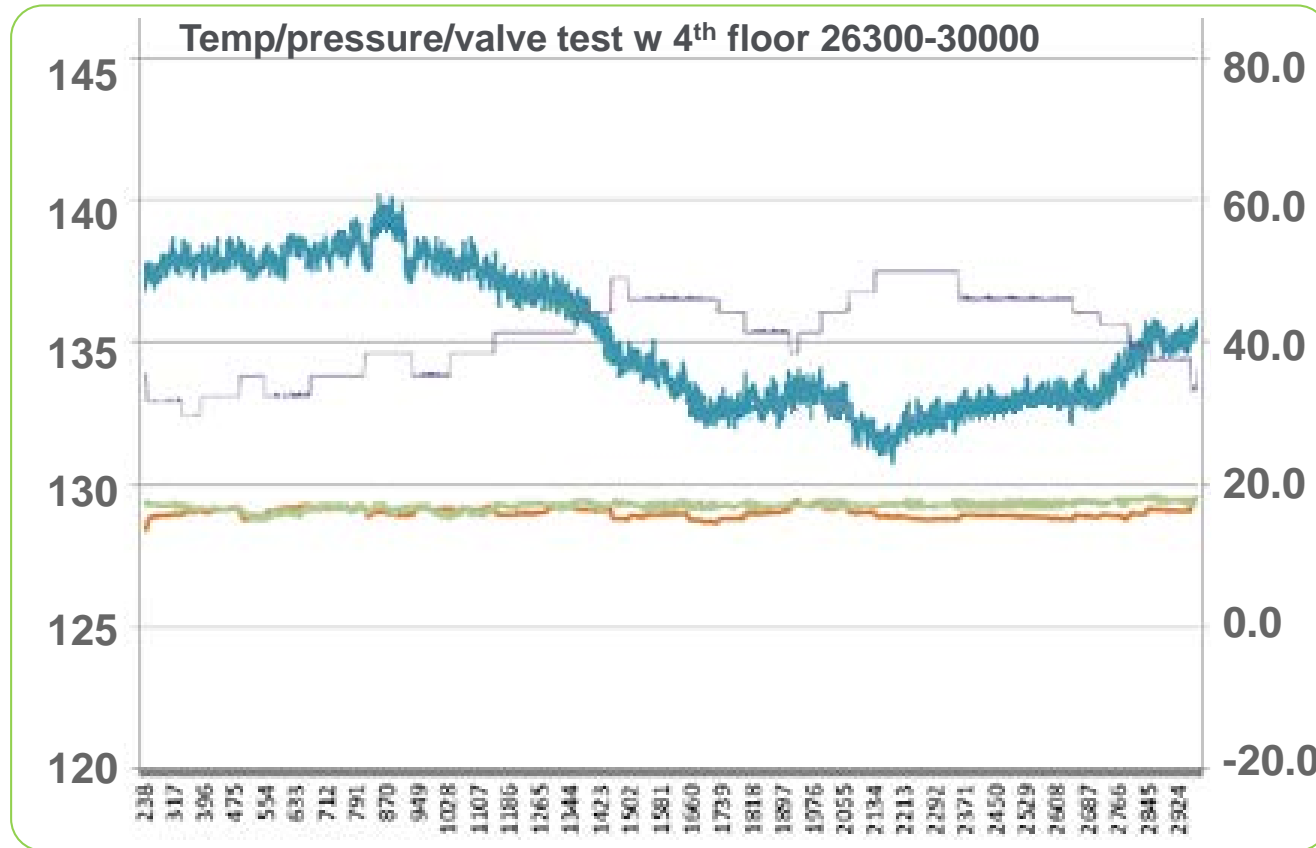


# Case Study



- Demonstrated some AHU control problems
- Two floors:
  - 3rd floor AHU kept existing conventional valves
  - 4th floor AHU retrofitted with PI valves

# Case Study



3<sup>rd</sup> floor (conventional)

4<sup>th</sup> floor (PI valve)

3<sup>rd</sup> floor CHW Delta T

4<sup>th</sup> floor CHW Delta T

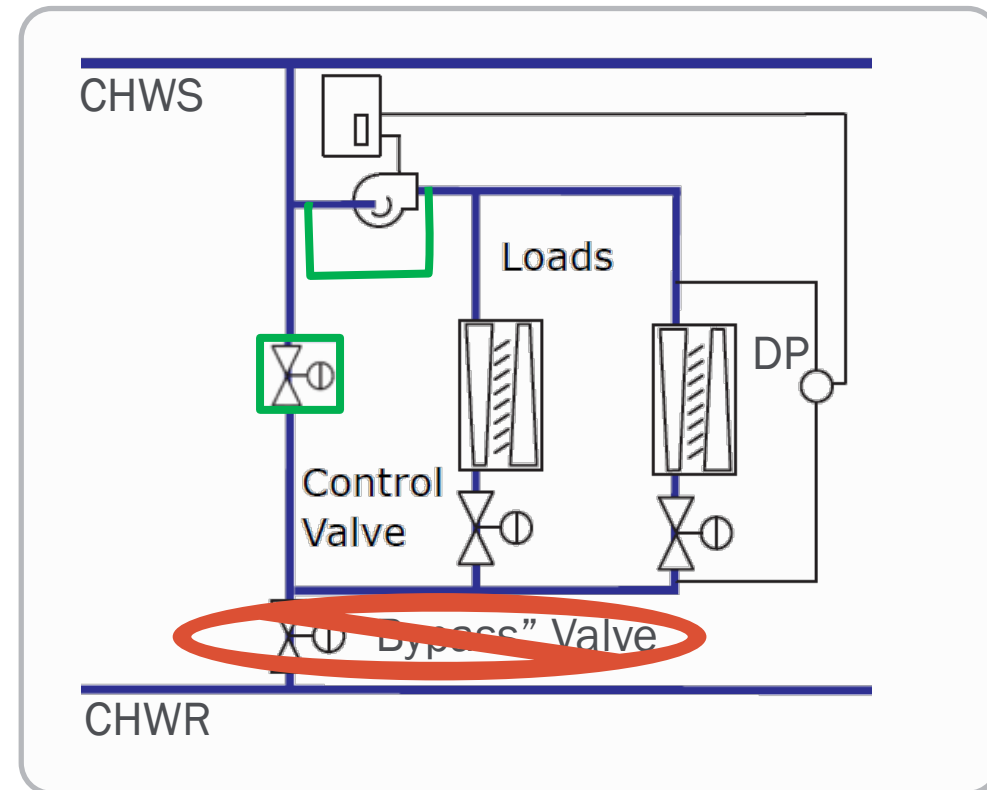
## Reason 5: Tertiary pumping

undesirable mixing is hard to prevent

1. 3-way control valves
2. LAT setpoint depression
3. Warmer chilled water
4. Deficient control valves
5. Tertiary pumping / bridge tender circuits

*Don't mix from the return,  
simply boost pressure*

- *Move bypass valve*
- *Bypass the pump  
(only use when needed)*



# Why is Low Delta-T Bad?

## Energy

- Excessive pump energy
- Increased chiller plant energy
  - More pumping energy
  - Chillers running at inefficient load points

## Capacity

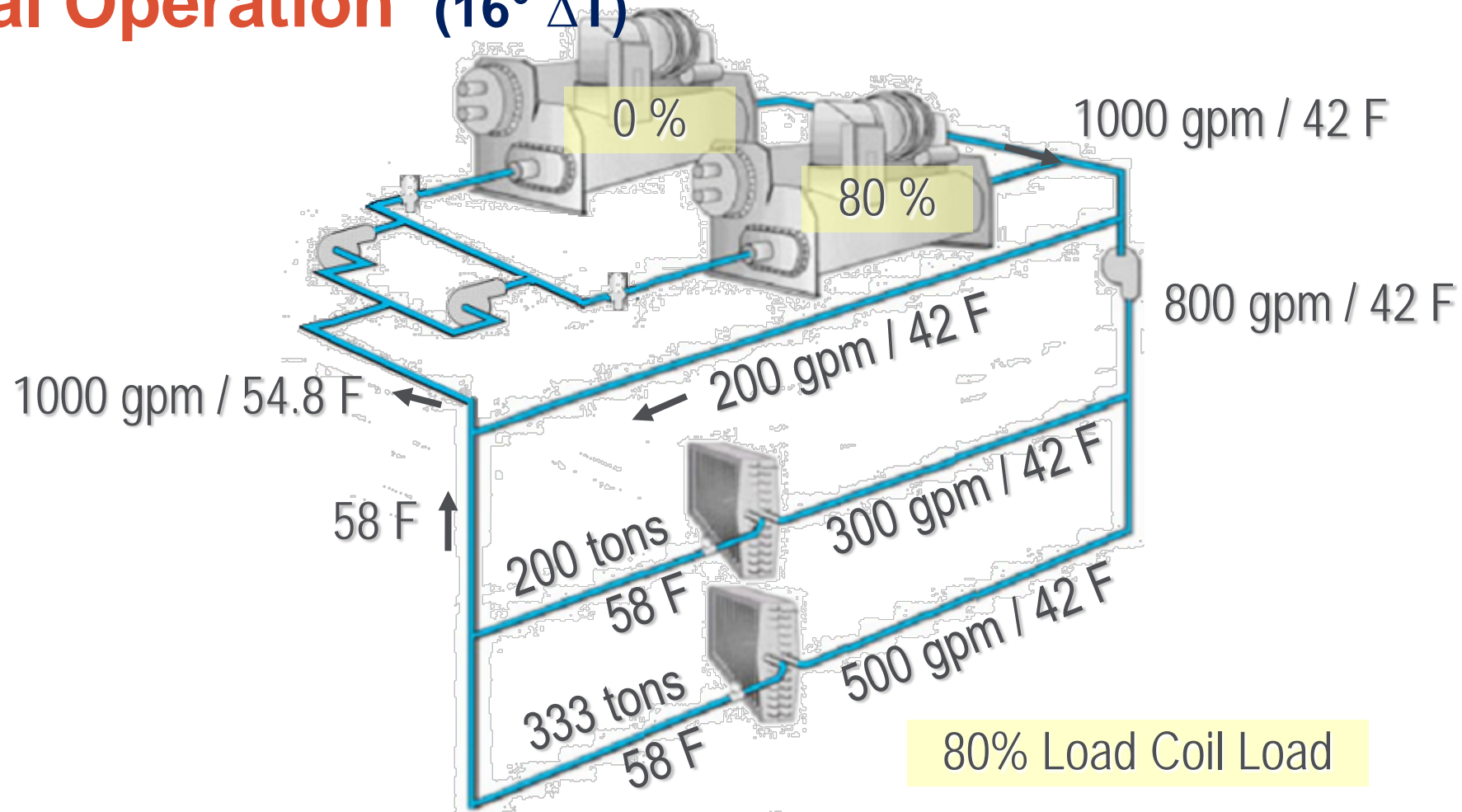
- Running out of distribution capacity
- Chiller won't load

Leads to overrides/manual operation

# Meanwhile in the Chiller Plant

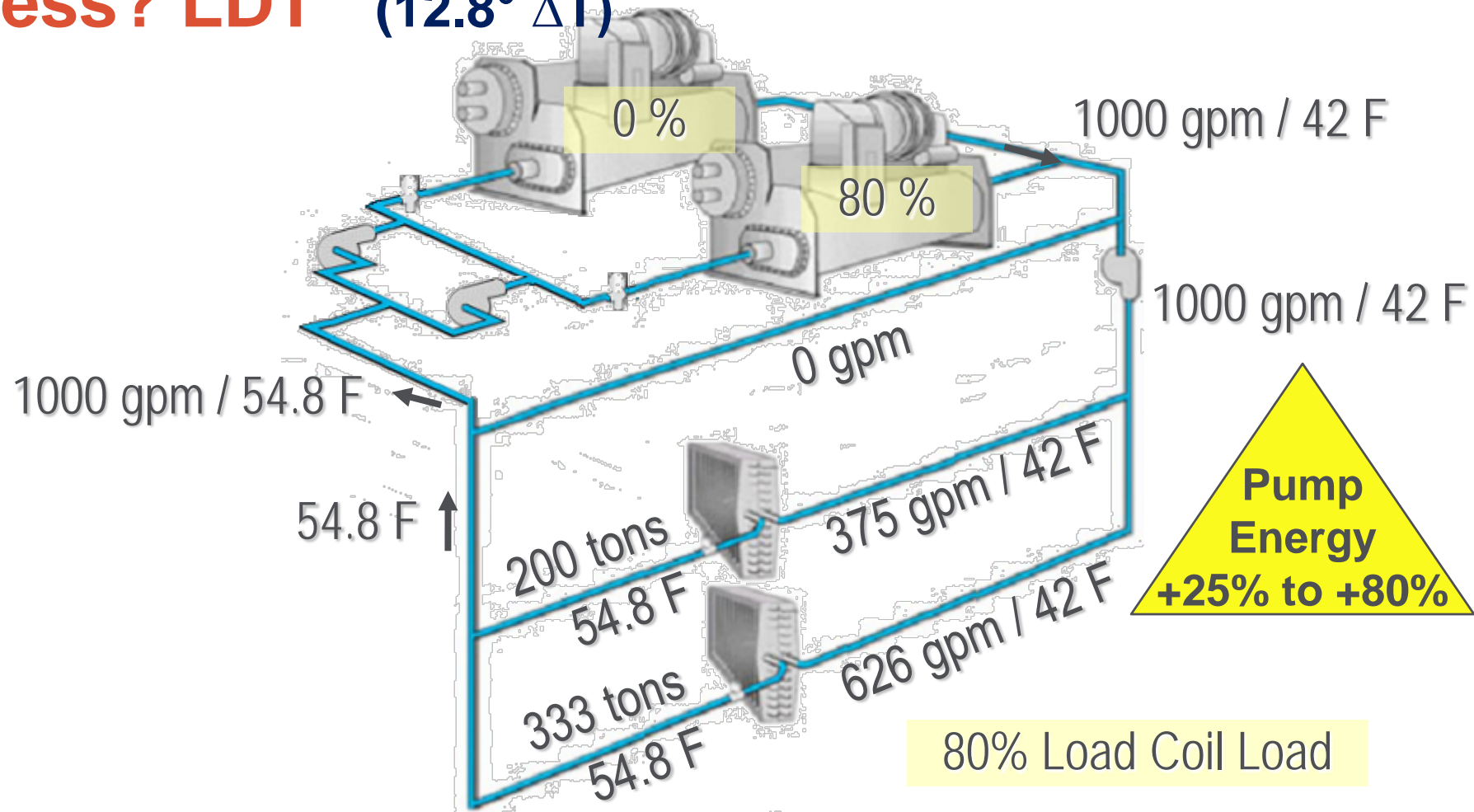
*Why is Low Delta T Bad for the chiller plant?*

## Normal Operation (16° ΔT)



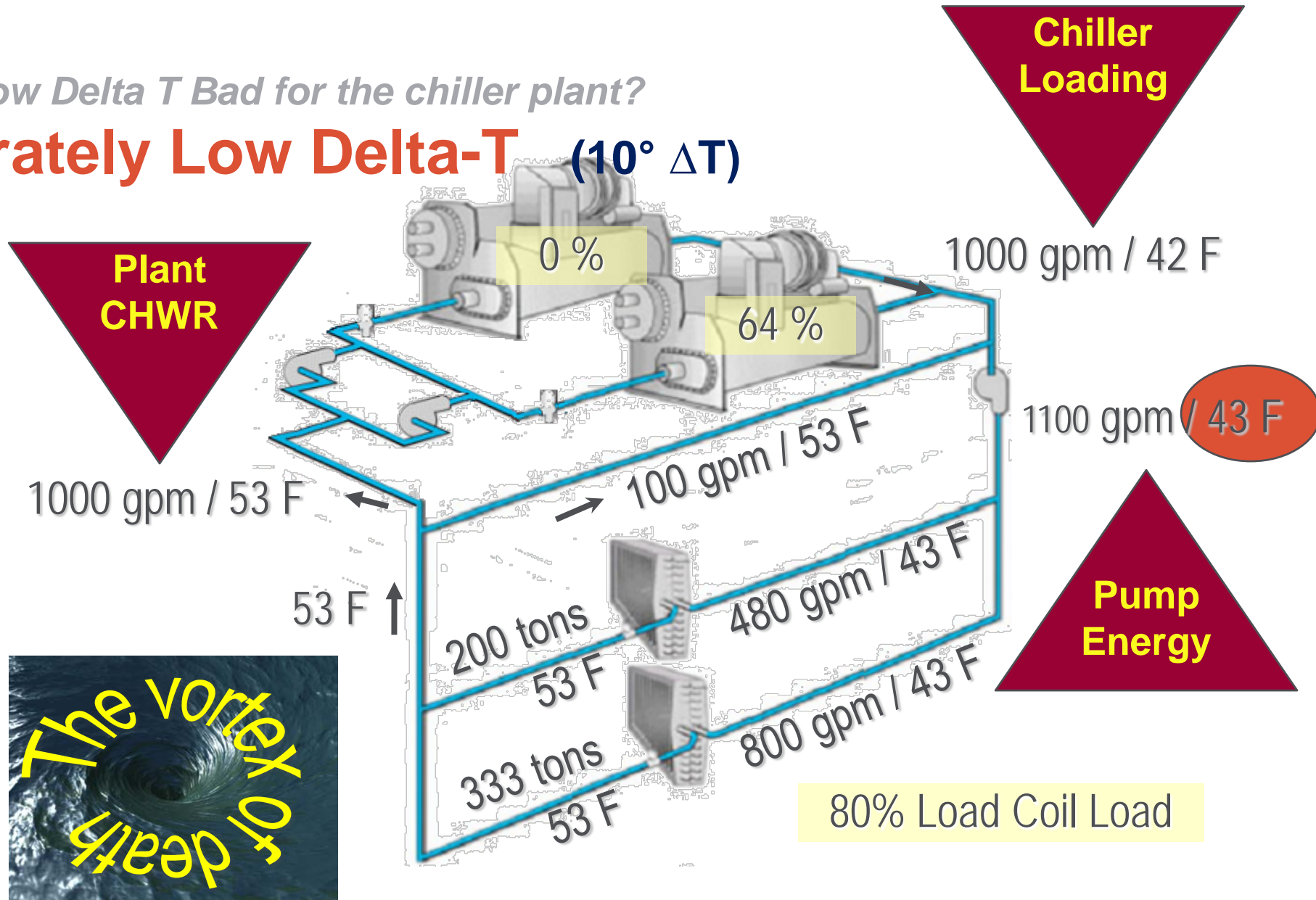
Why is Low Delta T Bad for the chiller plant?

**Harmless? LDT** (12.8°  $\Delta T$ )



Why is Low Delta T Bad for the chiller plant?

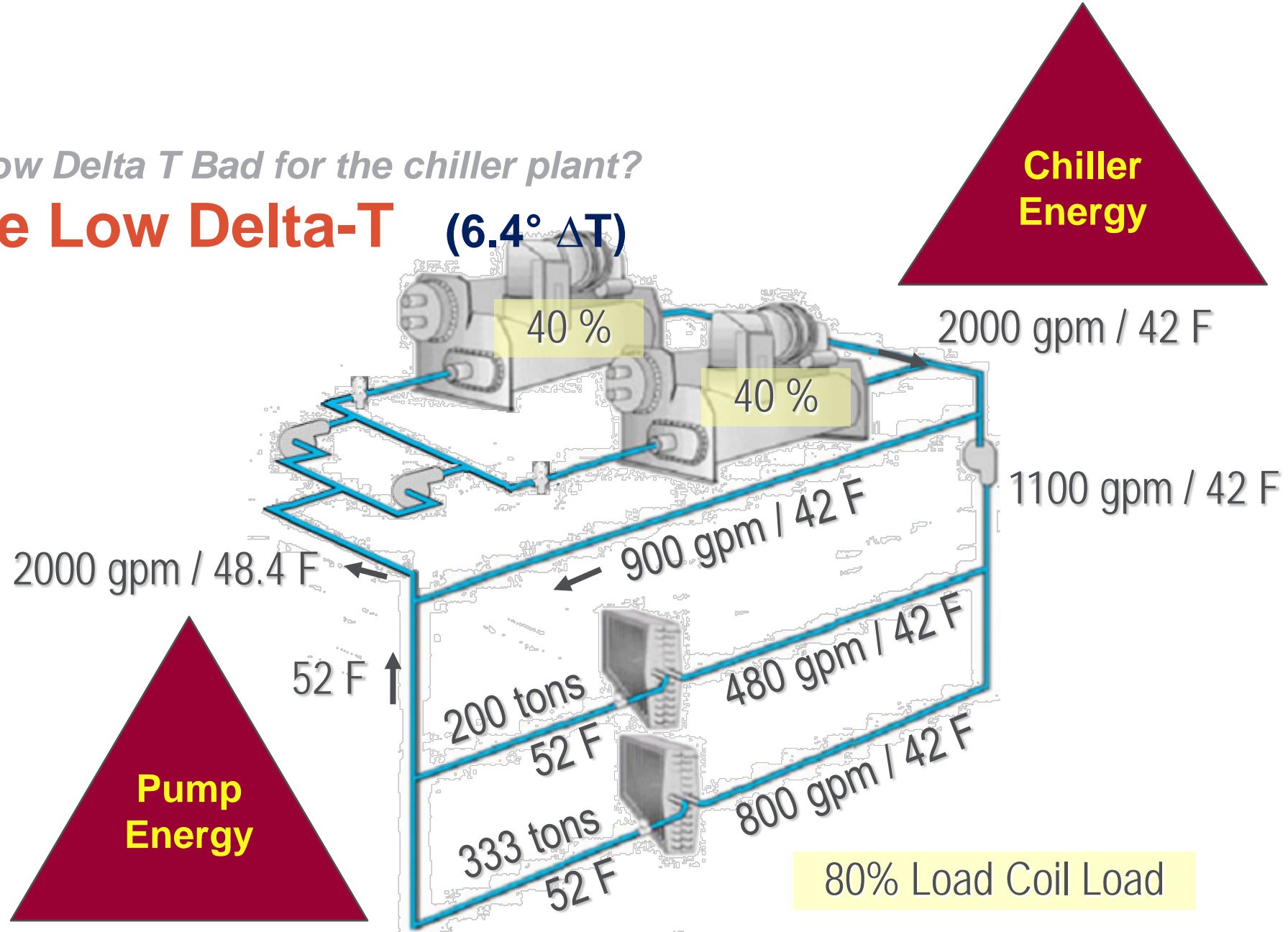
## Moderately Low Delta-T (10° ΔT)





Why is Low Delta T Bad for the chiller plant?

## Severe Low Delta-T (6.4° ΔT)



# Some Causes of Low Delta T

## Flow Control

- Three-way valves
- Cheap control valves
- Uncontrolled loads
- Excessive pump pressure
- Building “bridge circuits”

## Load

- Oversized coils
- Improper AHU setpoints

## Maintenance

- Dirty filters or coils
- Coils piped backwards

## Control

- Low AHU set points
- Unstable valve control
- Control calibration
- Improper CHW reset
- Diluted CHW supply temp

What is the number one thing you can do  
to improve the performance  
of a chiller plant?

**FIX THE THINGS  
OUTSIDE THE PLANT**



## Low Delta-T Syndrome

### **Some Band-Aids...**

- Lower the chiller's setpoint
  - Existing chiller maybe can – new chiller certainly can
  - Purchase new chillers that can work at harder than design conditions – also helps avoid surge and prepare for climate change
- Open the chiller balancing valves to allow more, “constant” flow to the chillers
- Convert to Variable Primary Flow
  - From constant flow this will be replacing valves
- Convert to Variable Primary / Variable Secondary
  - From primary-secondary flow this will be adding drives and maybe new pumps

# Summary

- Most energy can be saved in operation
  - All systems require attention to maintain peak performance
- Bake high efficiency into the design
  - Pick the right heat exchangers (coils, chillers, towers) with high  $\Delta T$
  - Use PIC valves
  - Get extra chiller 'lift' capability rather than excessive spare tons
- Harvest more data and turn it into intelligence
  - Find and remove overrides that are unhelpful
  - Trend and review at regular intervals

**Questions...**